# Vidyavardhini's College of Engineering and Technology 

Sample Paper TE Mechanical/ (R-2016)/ semester V/ Heat Transfer/ University of Mumbai Online Examinations January 2021
Section 1: Personal details
Section 2: MCQ (20 question 2 marks each, all compulsory)

| Q1. | The radial heat transfer rate through hollow cylinder increases as the ratio of outer radius to inner radius <br> (a) decreases <br> (b) increases <br> (c) constant <br> (d) none of the above. |
| :---: | :---: |
|  | Answer: a |
| Q2 | Conduction is a process of heat transfer from <br> (a) a hot body to a cold body, in a straight line, without affecting the intervening medium <br> (b) one particle of the body to another without the actual motion of the particles <br> (c) one particle of the body to another by the actual motion of the heated particles <br> (d) none of the above. |
|  | Answer: b |
| Q3 | The overall coefficient of heat transfer is used in the problems of <br> (a) radiation <br> (b) conduction <br> (c) convection <br> (d) conduction and convection. |
|  | Answer: d |
| Q4 | If $k$ is the thermal conductivity, $\rho$ is the mass density and $c$ is the specific heat then the thermal diffusivity of substance is given by <br> (a) $\frac{\rho c}{k}$ <br> (b) $\frac{k}{\rho c}$ <br> (c) $\frac{k c}{\rho}$ <br> (d) $\frac{k \rho}{c}$. |
|  | Answer: b |


| Q5 | In transient heat conduction, the two significant dimensionless parameters are $\qquad$ number and $\qquad$ number. <br> (a) Fourier, Reynolds <br> (b) Reynolds, Prandtl <br> (c) Biot, Fourier <br> (d) Reyonlds, Biot. |
| :---: | :---: |
|  | Answer: d |
| Q6 | The degree of approach, in heat exchangers, is defined as the difference between temperatures of <br> (a) hot medium outlet and cold water outlet <br> (b) hot medium outlet and cold water inlet <br> (c) cold water inlet and outlet <br> (d) hot medium inlet and outlet. |
|  | Answer: a |
| Q7 | $\qquad$ is the ratio of total emissive power of body to total emissive power of a black body at the same temperature. <br> (a) Emissivity <br> (b) Absoptivity <br> (c) Transmissivity <br> (d) Reflectivity. |
|  | Answer: a |
| Q8 | For infinite parallel planes with emissivities $e_{1}$ and $\mathrm{e}_{2}$, the interchange factor for radiation from surface 1 to surface 2 is <br> (a) $\frac{1}{\varepsilon_{1}+\varepsilon_{2}}$ <br> (b) $\varepsilon_{1}+\varepsilon_{2}$ <br> (c) $\varepsilon_{1}-\varepsilon_{2}$ <br> (d) $\frac{\varepsilon_{1} \varepsilon_{2}}{\varepsilon_{1}+\varepsilon_{2}-\varepsilon_{1} \varepsilon_{2}}$. |
|  | Answer: d |


| Q9 | The relationship $\lambda_{\max } T=$ constant, between the temperature of a black body and the wavelength at which maximum value of monochromatic emissive power occurs is known as $\qquad$ law. <br> (a) Lambert's <br> (b) Kirchhoff's <br> (c) Planck's <br> (d) Wien's displacement. |
| :---: | :---: |
|  | Answer: d |
| Q10 | With regard to 'Fouling factor' which of the following statements is correct? <br> (a) It is used when a liquid exchanges heat with a gas <br> (b) It is used only in case of Newtonian fluids <br> (c) It is dimensionless <br> (d) It is virtually a factor of safety in heat exchanger design. |
|  | Answer: d |
| Q11 | Grashoff number has significant role in heat transfer by $\qquad$ <br> (a) conduction <br> (b) radiation <br> (c) natural convection <br> (d) forced convection. |
|  | Answer: c |
| Q12 | In convective heat transfer, the Nusselt number <br> (a) represents the ratio of viscous to inertia force <br> (b) signifies the velocity gradient at the surface <br> (c) is the ratio of molecular momentum diffusivity to thermal diffusivity <br> (d) is the ratio of conduction to convection resistance. |
|  | Answer: d |


| Q13 | In case of laminar flow over a plate, the convective heat transfer co-efficient <br> (a) decreases with increase in free stream velocity <br> (b) increases with distance <br> (c) increases if a higher viscosity fluid is used <br> (d) increases if a denser fluid is used. |
| :---: | :---: |
|  | Answer: d |
| Q14 | Conduction through hollow, radial one dimensional heat transfer is expressed as <br> (a) $Q=\frac{2 \pi l\left(t_{1}-t_{2}\right) k}{\log _{e} r_{2} / r_{1}}$ <br> (b) $Q=\frac{2 \pi l\left(t_{1}-t_{2}\right)}{k\left(r_{2}-r_{1}\right)}$ <br> (c) $Q=\frac{2 \pi l \log _{e}\left(t_{1} / t_{2}\right)}{\left(r_{2}-r_{1}\right) k}$ <br> (d) $Q=\frac{2 \pi l\left(t_{1}-t_{2}\right) k}{\log _{e} r_{2} / r_{1}}$. |
|  | Answer: a |
| Q15 | For spheres, the critical thickness of insulation is given by <br> (a) $\frac{h}{2 k}$ <br> (b) $\frac{2 k}{h}$ <br> (c) $\frac{k}{h}$ <br> (d) $\frac{k}{2 \pi h}$ <br> where $k=$ thermal conductivity, $h=$ convective heat transfer coeffecient. |
|  | Answer: b |


| Q16 | Compared to parallel flow heat exchanger, LMTD in case of counter-flow heat exchanger is <br> (a) lower <br> (b) higher <br> (b) same <br> (d) unpredictable. |
| :---: | :---: |
|  | Answer: b |
| Q17 | In $\qquad$ flow maximum heat transfer rate can be expected. <br> (a) laminar <br> (b) turbulent <br> (c) counter current <br> (d) co-current. |
|  | Answer: b |
| Q18 | Why are baffles provided in heat exchangers ? <br> (a) To reduce heat transfer rate <br> (b) To increase heat transfer rate <br> (c) To remove dirt <br> (d) To reduce vibrations. |
|  | Answer: b |
| Q19 | On which of the following factors does the heat flux in nucleate pool boiling depend? <br> (a) Material of the surface only <br> (b) Material and roughness of the surface <br> (c) Liquid properties and material of the surface <br> (d) Liquid properties, material and condition of the surface. |
|  | Answer: d |
| Q20 | Which of the following terms does not pertain to radiation heat transfer? <br> (a) Configuration factor <br> (b) Spectral distribution <br> (c) Solid angle <br> (d) Reynolds analogy. |
|  | Answer: d |
| Section 3: Attempt any 4 out of 5. (10 marks each) |  |
| Q1) A longitudinal copper fin ( $\mathrm{k}=380 \mathrm{~W} / \mathrm{m}^{\circ} \mathrm{C}$ ) 600 mm long and 5 mm diameter is exposed to air stream at $20^{\circ} \mathrm{C}$. The convective heat transfer coefficient h is $20 \mathrm{~W} / \mathrm{m}^{2 \circ} \mathrm{C}$. If the fin base temperature is $150^{\circ} \mathrm{C}$, |  |

determine: i) the heat transferred in $\mathrm{kJ} / \mathrm{h}$ and ii ) the efficiency of the fin. Assume that fin is insulated at the tip.

Q2) Air at $27^{\circ} \mathrm{C}$ is flowing across a tube with a velocity of $25 \mathrm{~m} / \mathrm{s}$. The tube could be either a square of 5 cm side or a circular cylinder of 5 cm diameter.
Compare:
the rate of heat transfer in each case, if the tube surface is at $127^{\circ} \mathrm{C}$.
Use Nu= $\mathrm{C}(\operatorname{Re})^{\mathrm{n}}(\operatorname{Pr})^{1 / 3}$.,
Where, $\mathrm{C}=0.027$, $\mathrm{n}=0.805$ for cylinder, $\mathrm{C}=0.102, \mathrm{n}=0.675$ for square tube.
Properties of air at $77^{\circ} \mathrm{C}$, $\rho=0.955 \mathrm{~kg} / \mathrm{m}^{3}, \mathrm{k}_{\mathrm{f}}=0.03 \mathrm{~W} / \mathrm{mk} . \mathrm{K}, \mathrm{v}=20.92 \times 10^{-6} \mathrm{~m}^{2} / \mathrm{s}, \operatorname{Pr}=0.7, \mathrm{C}_{\mathrm{p}}=1.009 \mathrm{~kJ} / \mathrm{kg} . \mathrm{K}$.

Q3) Show by dimensional analysis for forced convection, $\mathrm{Nu}=\varnothing$ (Re, Pr$)$

Q4) Steam in a condenser of a steam power plant is to be condensed at a temperature of $30^{\circ} \mathrm{C}$ with a cooling water from nearby lake, which enters the tube of condenser at $14^{\circ} \mathrm{C}$ and leaves at $22^{\circ} \mathrm{C}$. The surface area of the tubes is $45 \mathrm{~m}^{2}$ and an overall heat transfer coefficient is $2100 \mathrm{~W} / \mathrm{m}^{2}$.K. Calculate the mass flow rate of cooling water needed and rate of steam condensation in the condenser. Treat the condenser as counter flow heat exchanger. $\mathrm{C}_{\mathrm{p}}$ of water at $18^{\circ} \mathrm{C}$ is $4.18 \mathrm{~kJ} / \mathrm{kg} . \mathrm{K}$ and latent heat of vaporization at $30^{\circ} \mathrm{C}$ if $\mathrm{h}_{\mathrm{fg}}=2430.5 \mathrm{~kJ} / \mathrm{kg}$.

Q5) Calculate the net radiant heat exchange per $\mathrm{m}^{2}$ area for two parallel plates of temperature $427^{\circ} \mathrm{C}$ and $27^{\circ} \mathrm{C}$ respectively $\varepsilon$ (hot plate) $=0.9$ and $\varepsilon$ (cold plate) $=0.6$. If a polished aluminum shield is placed between them, find the \% reduction in heat transfer: $\varepsilon($ shield)=0.4.

